

CLAIM SUMMARY DOCUMENT

1. Canceled
2. (Previously amended) The process according to claim 24, wherein the oxygenates and unsaturates are selected from the group consisting of normal alcohols, mono-olefins, and mixtures thereof.
3. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least 0.5 wt% normal alcohols as oxygenates.
4. (Original) The process of claim 3, wherein the normal alcohols boil in the range of from about 50°C to about 350°C.
5. Canceled
6. Canceled
7. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 5.0 wt % mono-olefins.
8. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 15.0 wt % mono-olefins.
9. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 25.0 wt % mono-olefins.
10. (Original) The process of claim 9, wherein the mono-olefins boil in the range of from about -105 to 350°C.

11. (Previously amended) The process of claim 24, wherein the Fischer-Tropsch hydrocarbon stream is a low-boiling fraction in a range from about -65°C to about 350°C.

12. Canceled

13. Canceled

14. Canceled

15. Canceled

16. (Previously amended) The process of claim 24, wherein the first hydrogen-containing gas is from a hydrogen production unit.

17. (Previously amended) The process of claim 24, wherein the first hydrogen-containing gas is recycled from a hydroprocessing operation.

18. (Previously amended) The process of claim 24, wherein the first hydrogen-containing gas is syngas.

19. Canceled

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22. Canceled

23. Canceled

24. (Previously amended) A process for hydroconversion of a Fischer-Tropsch hydrocarbon stream including oxygenates and hydrocarbon unsaturates with reduction in formation of heavy molecular weight products during heating, the process comprising:

- a) adding a first hydrogen-containing gas to the hydrocarbon stream sufficient to reduce the amount of heavy molecular weight products formed during heating as compared to a heated hydrocarbon stream without added hydrogen, to form a mixed stream;
- b) heating the mixed stream;
- c) adding a second hydrogen-containing gas to the heated mixed stream sufficient to effect hydroconversion of the mixed stream, to form a hydroconversion feed stream;
- d) heating the hydroconversion feed stream to reaction temperature; and
- e) hydroconverting the hydroconversion feed stream.

25. (Original) The process of claim 24, wherein the first hydrogen-containing gas is added in an amount less than about 500 Standard Cubic Feed per Barrel (SCFB).

26. (Original) The process of claim 25, wherein the first hydrogen-containing gas is added in an amount less than about 100 SCFB.

27. (Original) The process of claim 26, wherein the first hydrogen-containing gas is added in an amount less than about 50 SCFB.

28. (Original) The process of claim 24, wherein the second hydrogen-containing gas is added in an amount less than 750 SCFB.

29. (Previously amended) The process of claim 24, wherein the mixed stream is heated to a temperature in the range of from about 120°C to about 400°C.

30. (Original) The process of claim 24, wherein the mixed stream is heated to a temperature in the range of from about 250°C to about 400°C.